

Using Indoor Component Accelerated Stress Testing to Extrapolate to Outdoor Use



2nd Atlas/NIST Workshop on Photovoltaic Materials Durability

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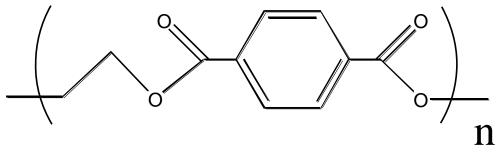
Introduction

- PV modules degrade in response to environmental stresses such as heat, humidity, UV irradiation, CTE mismatch, high voltage, and etc..
- Many degradation processes are driven by complex combinations of these stress factors.
- For some mechanisms, it is possible to quantify the governing kinetics and extrapolate long term performance.
- Getting highly predictive data is possible, but most accurate with narrow, well defined scope.

Outline

- Look at the hydrolysis of a typical back-sheet made of PET as a case study for comparing 85 °C/85% RH to outdoor exposure.
- Investigate moisture ingress modeling through edge-seal materials.
- Look at crystalline Si corrosion model extrapolating to outdoor use.
 - (uses data from Kent Whitfield et al. Formerly with Solaria).

PET Hydrolysis Modeling

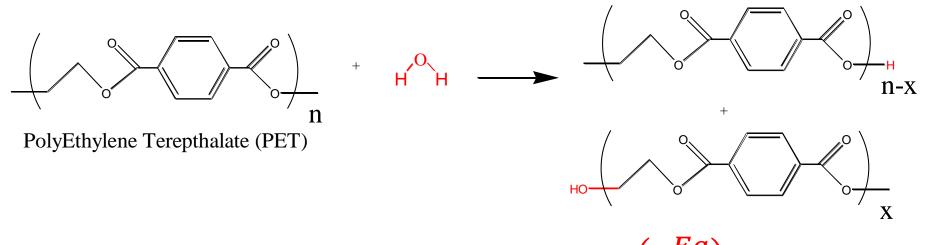


PolyEthylene Terepthalate (PET)

• PET is commonly used in back-sheet materials:

- Low cost
- Good electrical insulator
- Long term track record
- Hydrolysis results in embrittlement of PET which can lead to cracking and back-sheet failure.
- However, hydrolysis is only one potentially relevant failure mechanism.

PET Hydrolysis Kinetics



$$\log\left(\frac{C}{C-x}\right) = A \cdot t \cdot RH^2 \cdot e^{\left(\frac{-Ea}{kT}\right)}$$

Ea=130 kJ/mol (1.34 eV), $A=2.84 \cdot 10^{10}$ 1/day, *RH* expressed as a percentage.

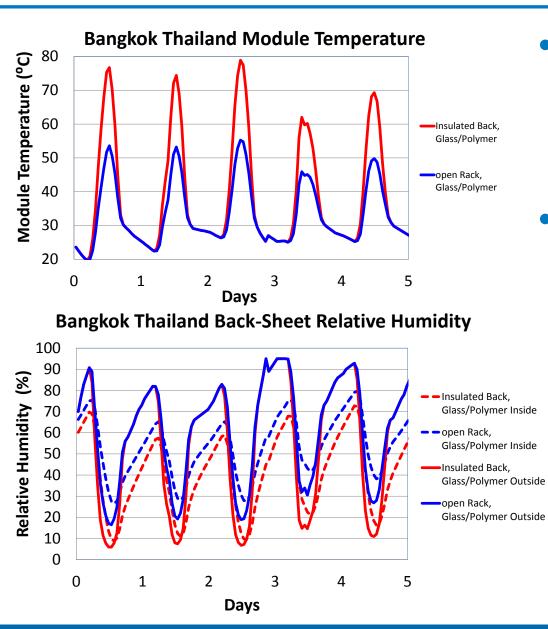
*PET becomes brittle (1/3 initial tensile strength) and "failed" when about 0.55% hydrolysis of ester bonds [log(C/C-x)=~0.0024].

*W. McMahon, H. A. Birdsall, G. R. Johnson, and C. T. Camilli, "Degradation Studies of Polyethylene Terephthalate," Journal of Chemical & Engineering Data, vol. 4, pp. 57-79, 1959.

**J. E. Pickett and D. J. Coyle, "Hydrolysis Kinetics of Condensation Polymers Under Humidity Aging Conditions," Polymer Degradation and Stability, vol. 98, pp. 1311-1320, 2013.

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Back-Sheet Exposure



• The back-sheet is dry when it is hot.

 To model PET hydrolysis, we used a RH that is an average of the inside and outside humidity to estimate the degradation of PET.

PET Hydrolysis Results

$$log\left(\frac{C}{C-x}\right) = A \cdot t \cdot RH^2 \cdot e^{\left(\frac{-Ea}{kT}\right)}$$

| | Years to 0.55% degradation (i.e. Hydrolysis Service Life) (y) | | 1000 Hours 85°C/85% RH Years equivalent (y) | | |
|-------------------------|------------------------------------------------------------------------|-----------|------------------------------------------------------|-----------|--|
| | Open | Insulated | Open | Insulated | |
| | Rack | Back | Rack | Back | |
| Denver, Colorado | 13,000 | 4,900 | 6,500 | 2,400 | |
| Munich, Germany | 11,000 | 4,400 | 5,100 | 2,100 | |
| Albuquerque, New Mexico | 9,000 | 3,200 | 4,400 | 1,500 | |
| Riyadh, Saudi Arabia | 8,200 | 3,000 | 4,000 | 1,500 | |
| Phoenix, Arizona | 3,400 | 1,300 | 1,700 | 630 | |
| Miami, Florida | 1,100 510 | | 530 | 250 | |
| Bangkok, Thailand | 700 | 310 | 320 | 150 | |

PET is predicted to "fail" (1/3rd initial tensile strength) after 2064 h of 85 °C and 85% RH.

Site Specific Equivalent T and RH

$$R = A \cdot RH^{n}e^{\left(-\frac{Ea}{kT}\right)}$$
$$T_{eq} = -\frac{Ea}{kln\left[\frac{\sum e^{\left(-\frac{Ea}{kT}\right)}}{N}\right]}$$

The equivalent temperature (T_{eq}) gives the temperature at RH_{WA} for which constant conditions will produce a degradation rate equivalent to the yearly average.

$$RH_{weighted average} = RH_{WA} = \left[\frac{\sum RH^{n}e^{\left(-\frac{Ea}{kT}\right)}}{\sum e^{\left(-\frac{Ea}{kT}\right)}}\right]^{\frac{1}{n}}$$

RH_{WA} is an average effective relative humidity weighted towards higher temperatures where most of the damage occurs.

PET Hydrolysis Equivalent T and RH

$$log\left(\frac{C}{C-x}\right) = A \cdot t \cdot RH^2 \cdot e^{\left(\frac{-Ea}{kT}\right)}$$

| | Years to 0.55% degradation (i.e. Hydrolysis Service Life) (y) | | 1000 Hours 85°C/85% RH Years equivalent (y) | | Teq for Ea=129.3 kJ/mol (°C) | | RH, at Teq for 2nd order Kinetics of PET (%) | |
|-------------------------|------------------------------------------------------------------------|-----------|------------------------------------------------------|-----------|---------------------------------|-----------|----------------------------------------------------|-----------|
| | Open | Insulated | Open | Insulated | Open | Insulated | Open | Insulated |
| | Rack | Back | Rack | Back | Rack | Back | Rack | Back |
| Denver, Colorado | 13,000 | 4,900 | 6,500 | 2,400 | 33 | 54 | 14 | 4.6 |
| Munich, Germany | 11,000 | 4,400 | 5,100 | 2,100 | 28 | 46 | 25 | 8.4 |
| Albuquerque, New Mexico | 9,000 | 3,200 | 4,400 | 1,500 | 37 | 58 | 13 | 4.2 |
| Riyadh, Saudi Arabia | 8,200 | 3,000 | 4,000 | 1,500 | 48 | 70 | 5.6 | 2.0 |
| Phoenix, Arizona | 3,400 | 1,300 | 1,700 | 630 | 46 | 68 | 9.8 | 3.3 |
| Miami, Florida | 1,100 | 510 | 530 | 250 | 37 | 54 | 36 | 14 |
| Bangkok, Thailand | 700 | 310 | 320 | 150 | 41 | 59 | 33 | 12 |

PET is predicted to "fail" (1/3rd initial tensile strength) after 2064 h of 85 °C and 85% RH.

85°C/85% RH is a Large Acceleration For PET

$$log\left(\frac{C}{C-x}\right) = A \cdot t \cdot RH^2 \cdot e^{\left(\frac{-Ea}{kT}\right)} \underbrace{\left(\frac{-Ea}{kT}\right)}_{\text{PolyEthylene Terepthalate (PET)}}$$

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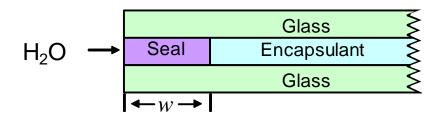
| | Teq for Ea=129 kJ/mol (°C) | | RH, at Teq for 2nd order Kinetics of PET (%) | | Acceleration Factor Relative to 85ºC/85% RH | |
|-------------------------|-------------------------------|-------------------|----------------------------------------------------|-------------------|---------------------------------------------------|-------------------|
| | Open Rack | Insulated Back | Open Rack | Insulated Back | Open Rack | Insulated Back |
| Denver, Colorado | 33 | 54 | 14 | 4.6 | 59000 | 22000 |
| Munich, Germany | 28 | 46 | 25 | 8.4 | 46000 | 19000 |
| Albuquerque, New Mexico | 37 | 58 | 13 | 4.2 | 39000 | 14000 |
| Riyadh, Saudi Arabia | 48 | 70 | 5.6 | 2.0 | 36000 | 13000 |
| Phoenix, Arizona | 46 | 68 | 9.8 | 3.3 | 15000 | 6000 |
| Miami, Florida | 37 | 54 | 36 | 14 | 4800 | 2000 |
| Bangkok, Thailand | 41 | 59 | 33 | 12 | 2900 | 1400 |

PET is predicted to "fail" (1/3rd initial tensile strength) after 2064 h of 85 °C and 85% RH.

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Edge Seal Modeling

- The use of fillers, pigments, and desiccants makes the determination of modeling parameters much more difficult.
 - -Each inorganic component will have unique absorption/desorption and diffusion characteristics.
 - -The polymer matrix may have its own temperature and RH dependent diffusivity and solubility parameters.
 - -Thus, a complete model would involve 10 to 20 adjustable parameters.



$$S_m = S_o e^{\left(-\frac{Ea_s}{kT}\right)} \frac{RH\%}{100\%}$$

Mobile phase water absorption is split between the polymer matrix and the mineral components. Assume linearity with relative humidity.

$$D_{eff} = D_o e^{\left(-\frac{Ea_D}{kT}\right)}$$

Mobile phase water diffusivity is an effective diffusivity. This accounts for a rapid equilibration between adsorbed and dissolved water.

 R_{H_2O}

A non-reversible reaction with water that immobilizes the water.

Model Parameters: R_{H_2O} , S_o, Ea_s

 R_{H_2O}

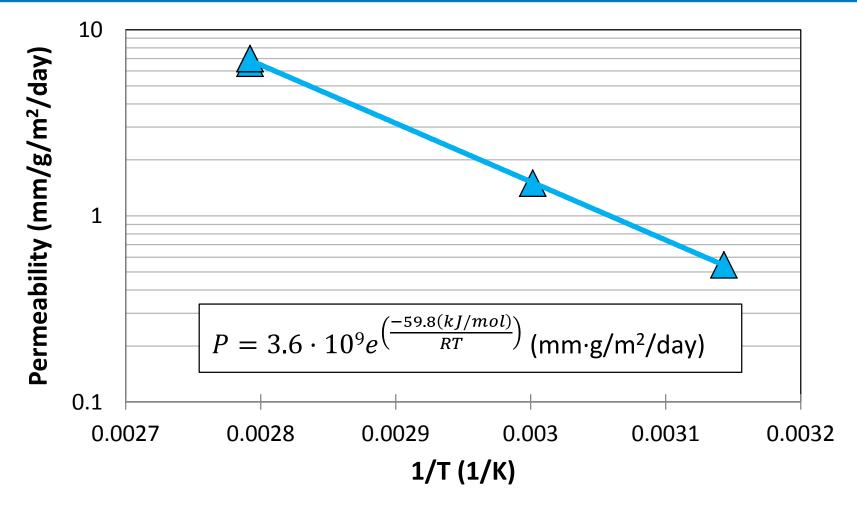
Measured by weighing samples before humidity exposure, after humidity exposure, and after drying. This gives values for both the reversible, *S*, and the irreversible moisture absorption, R_{H_2O} .

Measured by exposing material to controlled humidity, 85% RH at 45°C and 85°C, then drying in a TGA to determine reversible moisture loss. At both temperatures, values between 0.35 and 0.45% were obtained. This measurement was probably affected by adsorption on filler material and by loss of other volatile components.

A value of 5 kJ/mol was chosen as the lowest reasonable value, and S_o was set so S would be 0.35% at 45°C.

$$S_o$$
, Ea_s

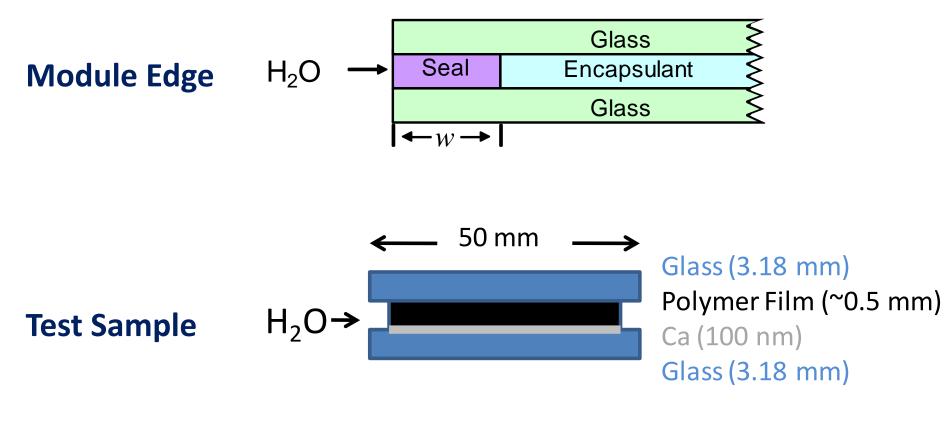
Model Parameter: Ea_D



Permeability=WVTR·thickness= $D \cdot S$ for Fickian materials. Therefore, as a first order approximation $Ea_D = Ea_P \cdot Ea_S$.

$$Ea_D = 54.8 \, kJ \,/ \,mol$$

Test Sample Designed to Mimic Module Edge

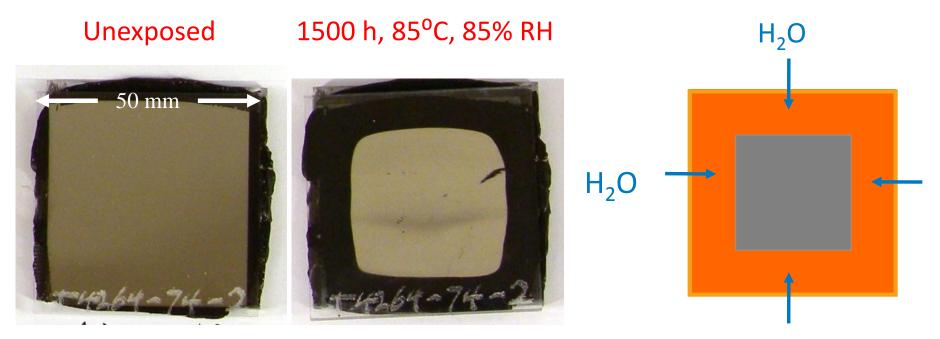


$Ca + 2 H_2 O \rightarrow Ca(OH)_2 + H_2$

Oxidation of Ca Indicates Moisture Ingress

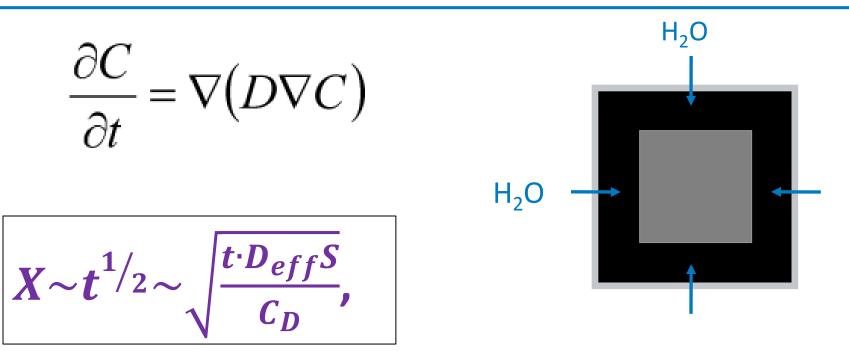


Mirror-Like → Transparent



Ca test samples PIB #2 based, desiccant filled edge seal. Samples are 50 mm by 50 mm.

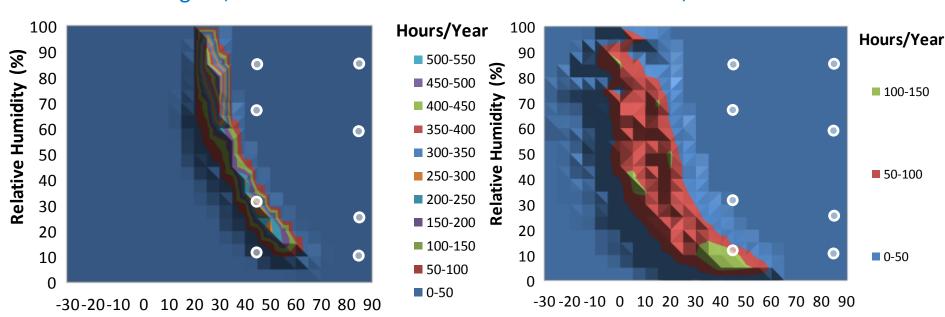
Moisture Ingress Rate Governed by Diffusion



Moisture ingress measured at 45°C and 85°C, with RH held at 85%, and at lower levels using saturated salt solutions of LiCl, MgCl, or NaNO₃.

| RH (%) | 45 | 85 |
|--------|------|------|
| | (°C) | (°C) |
| NaNO₃ | 67% | 59% |
| MgCl | 31% | 25% |
| LiCl | 11% | 10% |

Minimizing Extrapolation Reduces Uncertainty



Temperature (°C)

Bangkok, Thailand

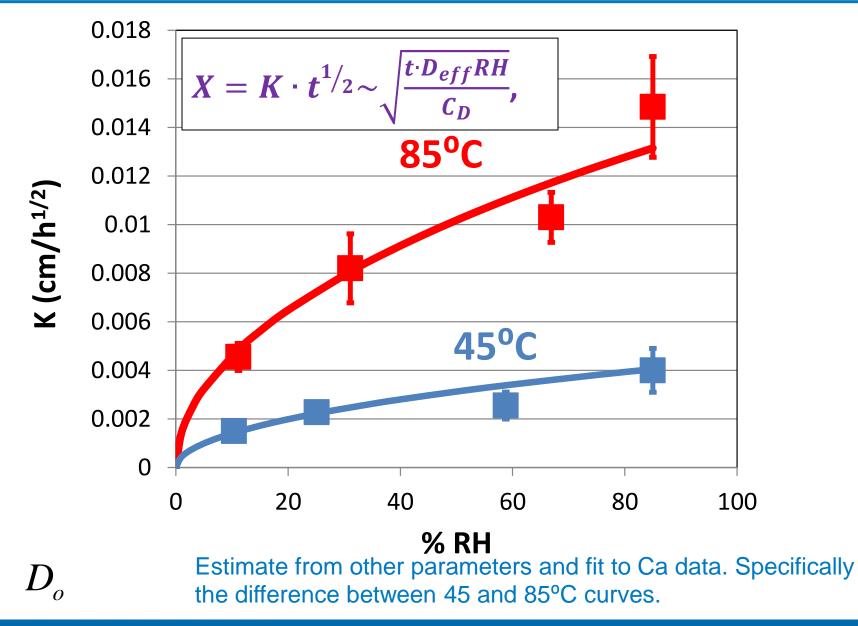
- 1. Conditions of 85°C and 85% RH are well beyond what will ever be seen in a deployed module.
- 2. Testing at low temperatures and low humidity takes an extremely long time, but it vital for reasonably minimizing extrapolation uncertainties.

| RH (%) | 45 | 85 |
|---------|------|------|
| NH (70) | (°C) | (°C) |
| NaNO₃ | 67% | 59% |
| MgCl | 31% | 25% |
| LiCl | 11% | 10% |

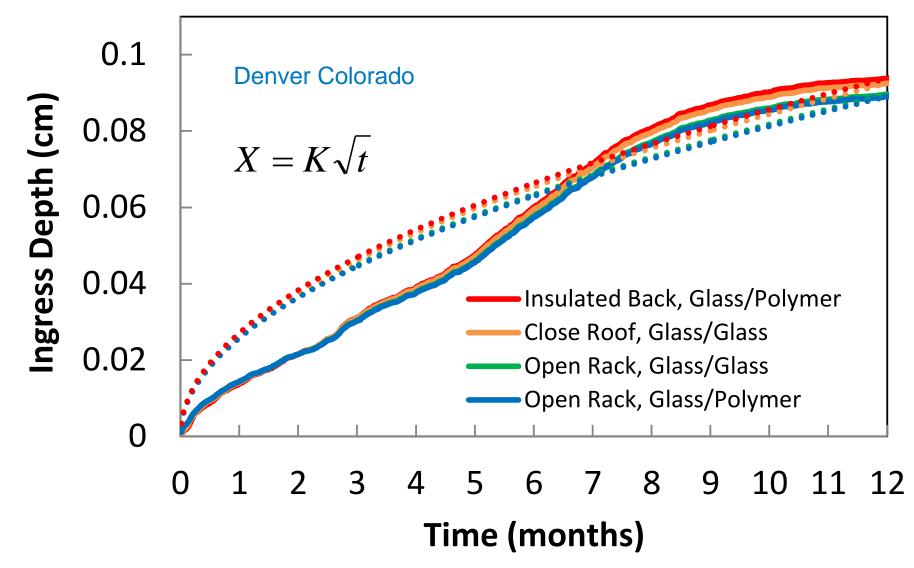
Denver, Colorado

Temperature (°C)

Permeation Measured at Low RH

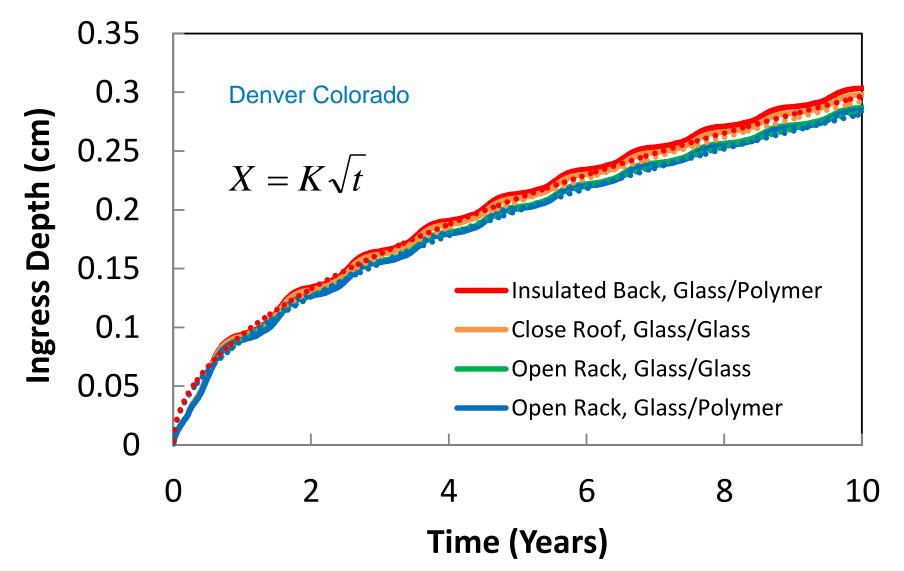


Ingress Estimated Using Finite Element Analysis



Used TMY3 Data and Temperature estimates similar to King et al, and Kurtz et al.

Square Root Relation Works to Longer Times



Used TMY3 Data and Temperature estimates similar to King et al, and Kurtz et al.

Results for Different Climates

| D _o (cm ² /s)= | $D_o(cm^2/s)=$ 0.33 | | | | Madalad 25 y | Madalad 25 y |
|--------------------------------------|---------------------|---------|----------------|----------------|---------------------------------|---------------------------------|
| Ea _p (kJ/mol)= | | 47 | Modeled K | Modeled 25 y | Modeled 25 y equivalent time | Modeled 25 y equivalent time |
| S _o (g/cm ³)= | | 0.16 | Modered K | required width | at 85°C/85% RH | at 45°C/85% RH |
| Ea _s (kJ/mol)= | = | 5 | | | | |
| Reactive Ca absorption | n (g/cm³)= | 0.047 | $(cm/h^{1/2})$ | (cm) | (h) | (years) |
| Denver, Colorado | Оре | en Rack | 0.00087 | 0.40 | 900 | 1.2 |
| Deriver, Cororado | Insulate | ed Back | 0.00103 | 0.44 | 1,000 | 1.4 |
| Munich, Germany | Open Rack | | 0.00096 | 0.45 | 1,100 | 1.5 |
| Municity Germany | Insulated Back | | 0.00107 | 0.47 | 1,200 | 1.7 |
| Riyadh, Saudi Arabia | Оре | en Rack | 0.00102 | 0.47 | 1,200 | 1.6 |
| myaan, sadar Arabia | Insulate | ed Back | 0.00124 | 0.51 | 1,400 | 1.9 |
| Phoenix, Arizona | Оре | en Rack | 0.00128 | 0.56 | 1,700 | 2.4 |
| Theenix, Anzona | Insulate | ed Back | 0.00153 | 0.61 | 2,000 | 2.8 |
| Miami, Flordia | Оре | en Rack | 0.00199 | 0.84 | 3,700 | 5.3 |
| Insulate | | ed Back | 0.00225 | 0.90 | 4,300 | 6.1 |
| Bangkok, Thailand | Оре | en Rack | 0.00228 | 0.96 | 4,900 | 6.9 |
| Dangkok, mananu | Insulate | ed Back | 0.00258 | 1.03 | 5,600 | 7.9 |

A sensitivity analysis gave about ±15% on K and Width, and ±30% on 25 yr equivalent time.

Parameters to Characterize an Environment

$$T_{eq} = \frac{-Ea}{k} \left(\frac{\sum_{i=0}^{n} e^{\left(\frac{-Ea_D}{kT_i}\right)}}{n} \right),$$

$$S_{DW} = \frac{\sum S \cdot RH \cdot D_{eff}}{\sum D_{eff}}$$

 The ability of the edge seal to take in water and hold it is related to the equilibrium solubility at the air/polymer interface and to the diffusivity. Therefore a diffusivity weighted solubility should describe a constant equivalent external water condition.

Simplified Equivalent Environment

| E | D _o (cm²/s)= a _b (kJ/mol)= | 17.0 54.8 | Modeled | T _{eq} | Diffusivity | RH at T _{eq} and | K at Diffusivity Weighted |
|-------------------------------------------------------------------|-----------------------------------------------------|--------------|------------------------|-----------------------|------------------------|---------------------------------------|----------------------------------|
| S _o (g/cm ³)= Ea _s (kJ/mol)= | | 0.0326 | К | using Ea _D | Weighted Solubility | Diffusivity Weighted Solubility | Temperature and Solubility |
| Reactive Ca absorpt | ion (g/cm³)= | 0.0320 | (cm/h ^{1/2}) | (°C) | (g/cm ³) | (%) | (cm/h ^{1/2}) |
| Denver, Colorado | (| Open Rack | 0.000864 | 23.2 | 0.00714 | 21.9 | 0.000874 |
| | Insul | ated Back | 0.000931 | 37.9 | 0.00276 | 8.5 | 0.000963 |
| Munich, Germany | Open Rack | | 0.000951 | 17.9 | 0.0136 | 41.8 | 0.000966 |
| Information, Oermany | Insul | ated Back | 0.00101 | 29.3 | 0.00623 | 19.2 | 0.00104 |
| Riyadh, Saudi | (| Dpen Rack | 0.00099 | 39.7 | 0.00275 | 8.5 | 0.00103 |
| Arabia | Insul | ated Back | 0.00108 | 55.7 | 0.00111 | 3.4 | 0.00114 |
| Decenix Arizona | (| Open Rack | 0.00120 | 37.9 | 0.00439 | 13.5 | 0.00122 |
| Phoenix, Arizona | Insul | ated Back | 0.00131 | 54.1 | 0.00174 | 5.3 | 0.00135 |
| Miami Elorida | (| Open Rack | 0.00179 | 32.2 | 0.0149 | 45.9 | 0.00180 |
| Miami, Florida | Insu | ated Back | 0.00192 | 43.6 | 0.00753 | 23.1 | 0.00196 |
| Depakok Thiologa | (| Open Rack | 0.00205 | 36.5 | 0.0140 | 43.1 | 0.00206 |
| Bangkok, Thialand | Insul | ated Back | 0.00219 | 48.2 | 0.00710 | 21.8 | 0.00224 |

Crystalline Silicon Metallization Corrosion

 Whitfield et al. measured cell performance of three different cell types at a variety of Temperatures and relative humidity levels.

| Condition | Cell | Temp. | Rel. Humidity |
|-----------|-------|-------|---------------|
| | Туре | (°C) | (%) |
| 1 | A/B/C | 85 | 85 |
| 2 | A/B/C | 110 | 100 |
| 3 | A/B/C | 120 | 100 |
| 4 | A/B/C | 125 | 100 |
| 5 | A/B/C | 130 | 80 |
| 6 | A/B/C | 130 | 90 |
| 7 | A/B/C | 130 | 95 |

Table 3 Design of experiments (DOE).

K. Whitfield, A. Salomon, S. Yang, I. Suez, "Damp Heat Versus Field Reliability for Crystalline Silicon", 38th IEEE PVSC, Austin TX, 2012.

Empirical Model Forms and Parameters

| Model | #1 _{Fa} | Model #2 | | | | |
|----------------------------------|----------------------------------|-----------------|---------------------------------------------------------|--|--|--|
| $Model$ $TF_1 = F_1 \cdot e^{c}$ | $E \cdot RH e^{\frac{Lu_1}{kT}}$ | T | $Model \#2$ $TF_2 = F_2 \cdot RH^b e^{\frac{Ea_2}{kT}}$ | | | |
| | Exponer | ntial Corrosion | Model | | | |
| Cell | F1 (hr) | C (no units) | Ea1 (eV) | | | |
| А | 1.13E-04 | -3.03 | 0.595 | | | |
| В | 7.47E-05 | -2.62 | 0.597 | | | |
| С | 5.77E-05 | -5.42 | 0.677 | | | |
| | Ро | wer Law Mode | el | | | |
| Cell | F2 (hr) | b (1/%) | Ea2 (eV) | | | |
| А | 1.824 | -2.77 | 0.596 | | | |
| В | 0.320 | -2.39 | 0.597 | | | |
| С | 1884 | -4.95 | 0.677 | | | |

Table 4Best fit acceleration model parameters.

K. Whitfield, A. Salomon, S. Yang, I. Suez, "Damp Heat Versus Field Reliability for Crystalline Silicon", 38th IEEE PVSC, Austin TX, 2012.

Differentiation by Extrapolation to Use Environment

| | Cell Me | Cell Metallization Corrosion, Open Rack Glass/Polymer Module | | | | | | | |
|-----------------|---------|--------------------------------------------------------------|-------|--------|--------------|--------|--|--|--|
| | | Time to Failure (y) | | | | | | | |
| | Мос | del 1, Exponer | ntial | Mode | l 2, Power L | aw | | | |
| | Cell A | Cell A Cell B Cell C C | | | Cell B | Cell C | | | |
| Denver | 62 | 62 | 454 | 276.5 | 200 | 1798.4 | | | |
| Albuquerque | 50 | 50 | 430 | 372.9 | 245 | 3818.1 | | | |
| Miami | 17 | 17 | 59 | 27.9 | 23 | 88.8 | | | |
| Phoenix | 27 | 27 | 237 | 292.9 | 186 | 2986.6 | | | |
| Munich | 53 | 53 | 202 | 90.0 | 77 | 277.8 | | | |
| Bangkok | 13 | 13 | 48 | 23.5 | 19 | 77.8 | | | |
| Riyadh | 27 | 27 | 272 | 521.2 | 341 | 3070.6 | | | |
| 85°C/85% RH (h) | 2029 | 2027 | 1936 | 2010.3 | 1970.8 | 1782.4 | | | |

 The worst cell at 85°C/85% RH was predicted to be the best.

Acceleration Factors Vary Widely

| Acceleration Factors | PET | Edge Seal | Cell C Corrosion Kinetics | | |
|----------------------------|------------|---------------------|---------------------------|-----------------------|--|
| Open Rack Glass/Polymer | Hydrolysis | Moisture Ingress | Model 1, Exponential | Model 2, Power Law | |
| Denver, Colorado | 59000 | 250 | 2057 | 5134 | |
| Munich, Germany | 46000 | 200 | 913 | 793 | |
| Riyadh, Saudi Arabia | 36000 | 180 | 1233 | 8766 | |
| Phoenix, Arizona | 15000 | 130 | 1073 | 8526 | |
| Miami, Florida | 4800 | 58 | 266 | 254 | |
| Bangkok, Thailand | 2900 | 45 | 216 | 222 | |

85/85 Stress Testing

Conclusion

- To have accurate accelerated stress tests, you must use small acceleration factors or know the kinetics very well.
- It is likely that each degradation mechanism will have different activation energies.
- Different degradation kinetics can have significantly different responses in a given environment.
- Keeping acceleration close to use conditions and at low values will decrease the associated uncertainty.

Sarah Kurtz David Miller Peter Hacke

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