

# Gold nanorod separation and characterization by asymmetric-flow field flow fractionation with UV–Vis detection

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**Abstract** The application of asymmetric-flow field flow fractionation (A4F) for low aspect ratio gold nanorod (GNR) fractionation and characterization was comprehensively investigated. We report on two novel aspects of this application. The first addresses the analytical challenge involved in the fractionation of positively charged nanoparticles by A4F, due to the interaction that exists between the negatively charged native membrane and the analyte. We show that the mobile phase composition is a critical parameter for controlling fractionation and mitigating the membrane-analyte interaction. A mixture of ammonium nitrate and cetyl trimethyl ammonium bromide at different molar ratios enables separation of GNRs with high recovery. The second aspect is the demonstration of shape-based separation of GNRs in A4F normal mode elution (i.e., Brownian mode). We show that the elution of GNRs is due both to aspect ratio and a steric-entropic contribution for GNRs with the same diameter. This latter effect can be explained by their orientation vector inside the A4F channel. Our experimental results demonstrate the relevance of the theory described by Beckett and Giddings for non-spherical fractionation (Beckett and Giddings, *J Colloid and Interface Sci* 186(1):53–59, 1997). However, it is shown that this theory has its limit in the case of complex GNR mixtures, and that shape (i.e., aspect ratio) is the principal material parameter controlling elution of GNRs in A4F; the apparent translational diffusion coefficient of GNRs increases with

aspect ratio. Finally, the performance of the methodology developed in this work is evaluated by the fractionation and characterization of individual components from a mixture of GNR aspect ratios.

**Keywords** Field flow fractionation · Gold · Nanoparticle · Nanorod · Shape separation · Hyphenated technique · Elution mechanism · Positive charge

## Introduction

Metallic nanorods have attracted increasing attention due to the ease of preparation, the large number of synthetic methods available, the high uniformity achievable, and control over the aspect ratio, which in turn is primarily responsible for controlling the optical properties [2, 3]. Gold is widely recognized as the most important noble metal nanomaterial due to its unique optical response and its potential use in catalytic, biosensing, nanomedicine and electronic applications [2, 4–9]. The development of well-controlled shapes and novel structures of gold nanoparticles has therefore developed into an emerging research topic in its own right. More specifically, gold nanorods (GNRs) have many fascinating properties and have been used in sensors, for information storage, and in a number of biomedical applications such as photothermal therapy [10–15].

While substantial research has been carried out to develop and utilize single GNRs and GNR ensembles as sensors, many important unexplored aspects and challenges remain before GNRs can be effectively used in practice. One of these challenges is the need to achieve sensitive and relevant in situ characterization of GNR shape and size distributions. It is in this context that advanced separation techniques coupled to multiple detection modalities can play a significant role. Chromatographic techniques, such as size

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exclusion chromatography (SEC), have been successfully utilized to separate GNR mixtures [16]. However, SEC is limited by low resolution and selectivity (based on size and shape) and also a poor recovery resulting from irreversible adsorption of GNRs onto the column packing material, even when surfactants are used in the mobile phase [16].

Recently asymmetric-flow field flow fractionation (A4F), a hydrodynamic chromatographic separation technique, has emerged as a high performance alternative capable of characterizing both spheroidal and high aspect ratio nano-objects [17–26]. Reports indicate that A4F is a promising technique due to its versatility, dynamic range and size-resolution potential. Additional advantages of A4F include the ability to couple with multiple detectors that provide complementary results on the size and shape of the analytes, and the potential for high recovery due to the absence of a stationary phase. Detectors typically used in conjunction with A4F include multi-angle light scattering (MALS) and quasi-elastic light scattering (QELS), which provide size-related information on the analytes (i.e., radius of gyration,  $R_g$ , hydrodynamic radius,  $R_h$ , and translational diffusion coefficient,  $D$ ). Also the shape- and size-dependent optical properties can be conveniently obtained by coupling with a diode array detector (DAD) that provides real-time UV–vis absorption spectra. Indeed UV–vis is a very useful tool for the characterization of optically active gold nano-objects, due to their characteristic surface plasmon resonance (SPR) bands. GNRs have two characteristic SPR bands, one due to the transverse oscillation of the electrons that appears around 520 nm and the other due to the longitudinal plasmon resonance appearing at longer wavelengths [27–30]. The transverse SPR band, which does not depend on the aspect ratio, occurs at the same or similar wavelength as the SPR for spheres of equivalent diameter [28]. In contrast, the wavelength of the longitudinal SPR band increases with increasing aspect ratio [31].

Despite the promising capabilities of A4F for fractionation and characterization of GNRs, the development and optimization of methodology remains largely unexplored. Herein, we report the results of a comprehensive investigation in which GNRs of relatively low aspect ratios (i.e., < 10) have been successfully fractionated based on their aspect ratio and simultaneously characterized both dimensionally and optically. We address major practical challenges for application of A4F to GNRs, such as the adverse effect of attractive GNR-membrane interactions; commercially available membranes for A4F generally carry a negative charge in aqueous media, and therefore only negatively charged or neutral nano-objects can be easily fractionated by A4F using an unmodified membrane. GNRs are typically positively charged as a result of a widely used synthesis route that depends on adsorption of cationic surfactants; hence, the analyte is absorbed onto the membrane surface resulting in

elution failure. The second challenge involves the morphological complexity characterized by the variation in aspect ratio. Consequentially, poor resolution for separation and low recovery must be overcome by controlling critical factors including the mobile phase composition, the channel/cross flow ratio, and wavelength limitations of the DAD. Indeed, the innovative aspect of this research is the novel fractionation capacity of A4F demonstrated by the successful separation of GNR components from a complex mixture, not based on size or length, but on the aspect ratio, regardless of the GNR surface charge state.

## Experimental

### Reagents

Ammonium nitrate ( $\text{NH}_4\text{NO}_3$ , 99 %) and cetyl trimethyl ammonium bromide (CTAB) were purchased from VWR (Bridgeport, NJ)<sup>1</sup> and used without further purification. GNRs in aqueous suspension were obtained from Nanopartz (Loveland, CO). Vendor provided information and material characteristics are summarized in Table 1; while electron microscopy images and UV–vis absorbance spectra for the as received stock solutions are provided in the [Electronic Supplementary Material](#) (Electronic Supplementary Material, see Figures S1 and S2, respectively). Deionized (DI) water was generated by an Aqua Solutions (Jasper, GA, USA) ultra-low TOC biological grade water purification system. All A4F mobile phases were passed through a 0.2  $\mu\text{m}$  regenerated cellulose filter from VWR. Stock solutions of ammonium nitrate and CTAB were prepared by dissolving the required amount in DI water (18  $\text{M}\Omega\cdot\text{cm}$ )

### Instrumentation and methods

The A4F system used in this study is an Eclipse 3+ (Wyatt Technology, Santa Barbara, CA). A 350  $\mu\text{m}$  thick spacer was used, and channel dimensions were 26.5 cm in length and from (2.1 to 0.6) cm in width. For all experiments, polyethersulfone (PES) membranes with a 10 kDa cut-off were used (Wyatt Technology). Flows (main flow and cross flow) were controlled with an Agilent Technologies (Santa Clara, CA) 1100 series isocratic pump equipped with a degasser (Gastorr TG-14, Flom Co., Ltd., Tokyo, Japan). In this study, considering the size range of GNRs, the main flow ( $V_p$ ) was fixed at 0.5  $\text{mL}\cdot\text{min}^{-1}$ . Injections were performed by a manual injection valve (Rheodyne 7725i, IDEX Corporation, Oak Harbor, WA) equipped with a 100  $\mu\text{L}$

<sup>1</sup> The identification of any commercial product or trade name does not imply endorsement or recommendation by the National Institute of Standards and Technology.

**Table 1** GNR material properties as reported by the commercial vendor. TSPR refers to the transverse mode plasmon resonance band and LSPR refers to the longitudinal mode

Product ID	Sample name <sup>a</sup>	Length (nm)	Diameter (nm)	Aspect ratio	pH	Zeta potential (mV)	TSPR peak (nm)	TSPR AU <sup>b</sup>	LSPR peak (nm)	LSPR AU <sup>b</sup>	Concentration (mgmL <sup>-1</sup> )
30-25-550	GNR1.4	34	25	1.4	3.2	+38.2	550	1.2	524	0.75	0.043
30-25-700	GNR3.1	77	25	3.1	3	+39	712	1.2	521	0.2	0.060
30-10-780	GNR3.8	38	10	3.8	4	+40	782	1	512	0.3	0.040
30-10-850	GNR4.4	44	10	4.4	4.2	+38	844	1.2	509	0.16	0.040

<sup>a</sup>Number is the reported aspect ratio of corresponding GNR

<sup>b</sup>Absorbance units (i.e.,  $\log I_0/I$  measured in a 1 cm pathlength cell)

stainless steel sample loop. The detection train consisted of a 1200 series UV–Vis absorbance DAD (Agilent Technologies) with a spectral range from (190 to 950) nm and a sampling rate of 20 Hz; a fiber optic based MALS detector (DAWN HELIOS, Wyatt Technology); a fiber optic based QELS detector at a scattering angle of 90° (DynaPro, Wyatt Technology). Data from the different detectors was collected and analyzed using Astra version 5.3.1.18 software (Wyatt Technology).

All measurements were conducted at (20±0.1) °C, but temperature was directly controlled only in the light scattering cell. Eluting samples were subject to ambient temperatures outside of this cell, where the ambient temperature was generally within 2°C of the experimental temperature. A 100 µL injection of bulk solution was performed for each sample. Discrete measurement results are reported as the mean with an associated uncertainty of one standard deviation (presented as an interval or error bar) based on typically 3 to 5 replicates performed under repeatability conditions. A4F traces represent the mean of 3 to 5 replicate injections, where the average coefficient of variation between replicate elutions is far less than 1 %.

#### Practical parameters of A4F theory

Two modes of elution are possible in A4F: viz. normal (or Brownian) and steric. The dominant mode is determined by the fractionation conditions (channel thickness and mobile phase) and the analyte size range. Considering the size range involved in the present study, the normal mode should be operative. The elution time in A4F normal mode is determined by the diffusion coefficient ( $D$ ) of the analyte (and through  $D$  by the hydrodynamic radius  $R_h$ , according to the well known Stokes-Einstein relationship) as shown in Eq. (1) [32]:

$$D = \frac{V_c \cdot \omega^2 \cdot R}{6 \cdot V_0 \cdot (1 - R)^{\frac{1}{3}}} \quad (1)$$

Here,  $V_0$  is void volume (m<sup>3</sup>) - determined experimentally by tracing unretained dissolved species,  $V_c$  is cross flow rate (m<sup>3</sup> s<sup>-1</sup>),  $\eta$  is viscosity of the mobile phase (kg m<sup>-1</sup> s<sup>-1</sup>),  $R$  is retention ratio defined as  $t_0/t_R$  (ratio between void time and retention time),  $\omega$  is channel thickness (m). When  $V_c$  is kept constant and retention time ( $t_R$ ) is sufficiently long (i.e.,  $0.03 < R < 0.1$ ), then Eq. (1) can be simplified to Eq. (2), yielding a simple linear relationship between  $D$  and  $R$ :

$$D = \frac{V_c \cdot \omega^2 \cdot R}{6 \cdot V_0} \quad (2)$$

Here, the retention ratio  $R$  is an appropriate parameter to judge the efficiency of the fractionation process. Generally,  $R$  should be in the range from 0.025 to 0.1 [32]. With  $R$  over 0.1 the approximation described by Eq. (2) cannot be applied, and with  $R$  below 0.025 the resolution decreases because of excessive sample zone broadening. This signal broadening is observed by an increase in the elution time range associated with a peak signal.

The recovery ( $R\%$ ), i.e., the ratio between recovered mass after analysis and injected mass, is expressed as:

$$R\% = \frac{S}{S_0} \cdot 100 \quad (3)$$

Here,  $S$  and  $S_0$  are the surface area under the peak signal with and without applying cross-flow, respectively.  $R\%$  permits the evaluation of the performance ability of the A4F system to fractionate analytes without significant loss of analyte or analytical information.

## Results and discussion

### Influence of the mobile phase composition

In the case of GNRs, and other positively charged nano-objects, a major challenge for A4F fractionation arises from

the fact that the membrane or accumulation wall (which provides cross flow) is typically negatively charged, and thus irreversible attachments can occur resulting in a noisy peak with low recovery, as is demonstrated in the [Electronic Supplementary Material](#) (see Figure S3). A convenient and adaptable method to resolve this issue is to optimize the mobile phase; another option is to chemically modify the membrane. Here we have chosen the former method, due to its simplicity and questions concerning the stability and homogeneity of chemically functionalized membranes. The mobile phase composition and ionic strength are the most important parameters for controlling or mitigating the interaction-repulsion of the analytes at the native membrane surface.

In general, the mobile phase in A4F should provide the same electrical polarity between analytes and the membrane surface. In order to control the elution of GNRs by controlling the interaction-repulsion with the membrane, it was proposed to add an inert salt ( $\text{NH}_4\text{NO}_3$ ) and to combine the salt with the cationic surfactant CTAB at different molarity percentages while maintaining the total mobile phase ionic strength constant at  $0.5 \text{ mmolL}^{-1}$  (as it was previously found optimal for gold nanoparticle fractionation—see Figure S3 in the [Electronic Supplementary Material](#)) [19]. The use of a simple salt in the A4F mobile phase allows screening of electrostatic repulsion between nanoparticles and the negatively charged membrane [19], where a balance is sought between overly repulsive interactions (leading to no retention, resulting in no fractionation) and no repulsion (resulting in poor recovery and the band broadening effect).

Our preliminary results indicated that CTAB was required in the mobile phase to provide some repulsive force between the membrane and GNRs (see section [Results and Discussion](#) in SI for further details), which are otherwise mutually attractive. However, we found that using CTAB alone resulted in too much repulsion between GNRs and the membrane, and therefore the analytes were unretained on the membrane and pre-eluted without sufficient fractionation. Hence, the challenge in this case was to find an appropriate ratio between  $\text{NH}_4\text{NO}_3$  and CTAB to afford an acceptable fractionation of GNRs without significant loss of material. For mobile phase optimization, several  $\text{NH}_4\text{NO}_3$ /CTAB ratios were tested, and Table 2 summarizes the  $R\%$  and  $R$  values obtained for the different GNRs in mobile phases prepared as a function of composition ratio. To reveal the best compromise between  $R\%$  and  $R$  with minimal instrumental variables,  $V_p$  and  $V_c$  were kept constant at  $0.5 \text{ mLmin}^{-1}$  and  $0.8 \text{ mLmin}^{-1}$ , respectively. In addition, associated fractograms for the different GNRs with the different mobile phase compositions summarized in Table 2 are presented in Fig. 1.

At low CTAB content (5 % of the total ionic strength, i.e.  $0.025 \text{ mmolL}^{-1}$ ), an improvement of the signal was

observed for *GNR1.4* and *GNR3.1* compared to the signals obtained with only  $0.5 \text{ mmolL}^{-1}$  of  $\text{NH}_4\text{NO}_3$  (see [Electronic Supplementary Material](#), Figure S3). Nevertheless, the recovery obtained was unacceptably low, especially for *GNR3.8* and *GNR4.4*. These low recoveries are due to attractive interactions between GNRs and the accumulation wall membrane. The corresponding fractograms for these two GNRs confirmed the strong interactions based on the noisy and broadened signals (Fig. 1a). The CTAB quantity in this mobile phase system is too low to create sufficient repulsion between GNRs and the membrane (negatively charged surface). By increasing the proportion of CTAB in the mobile phase, it appears that the recovery reaches a maximum for all GNR samples at a ratio 30 %:70 % (CTAB: $\text{NH}_4\text{NO}_3$ ) while simultaneously the retention ratio increases. Clearly, this retention ratio increase is due to the increasing repulsion between GNRs and the membrane afforded by the increasing load of CTAB associated with the membrane surface. On the other hand, when the concentration of CTAB is over  $0.25 \text{ mmolL}^{-1}$ , a decrease in recovery appears due to the loss of materials through pre-elution (note this is not due to membrane attachment), and this effect is promoted by excessive repulsive interactions due to high CTAB concentration (see Section 3 in the [Electronic Supplementary Material](#), Figures S4 and S5). This puts an upper limit on the concentration with respect to recovery.

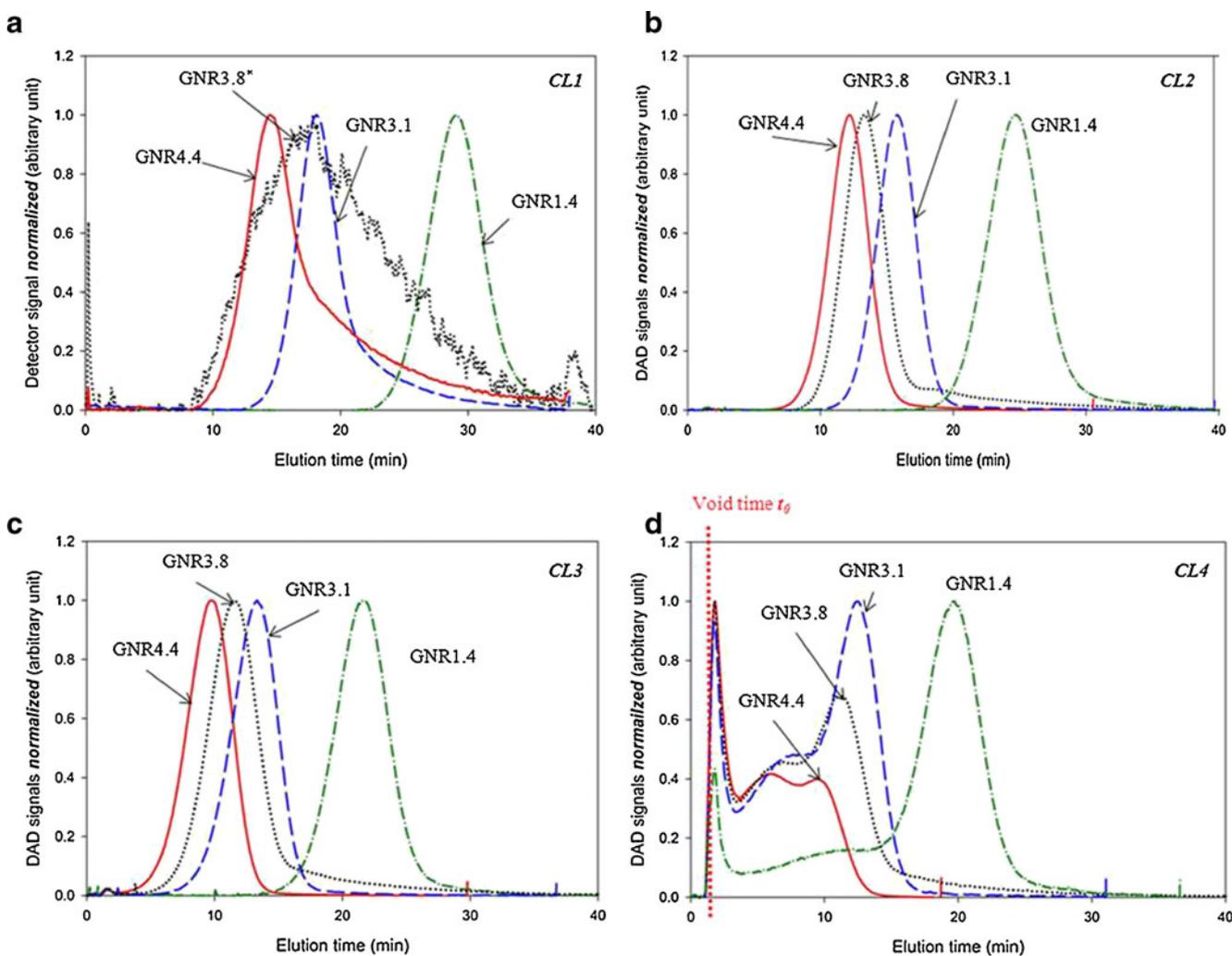
A4F fractograms for all GNR samples with mobile phase composition ratio of 70 %:30 % (CTAB: $\text{NH}_4\text{NO}_3$ ) are characterized by three distinguishable peaks (Fig. 1d), which indicates the complexity of GNR-membrane interactions at higher CTAB concentrations and suggests the formation of secondary structures. The first relatively small peak localized at the void time can be explained by strong repulsion between analytes and the membrane surface leading to a pre-elution of partially unretained GNRs, as previously observed by using CTAB exclusively in the mobile phase and explained further in the [Electronic Supplementary Material](#) (see Figure S4). The other characteristic signals that appear at retarded retention times show a signal splitting pattern most likely associated with the major peak of retained analyte. It is not yet fully clear, but presumably these splitting signals (even for monodisperse samples) might be due to a very sensitive response by A4F, either to the degree of interaction that occurs inside the channel between analyte and the accumulation wall or to the slight differences of sample components that possibly result from the manufacturing process.

From the results presented thus far, it appears that the best compromise is obtained for the CL2 mobile phase, containing 30 % CTAB and 70 % of  $\text{NH}_4\text{NO}_3$ . This mobile phase composition allows the highest recovery values ( $R\%$ ) and a reasonable retention ratio ( $R$ ) ranging from 0.035 to

**Table 2** Recovery and retention ratio obtained for the four GNRs with a selection of mobile phase compositions tested at an ionic strength of  $0.5 \text{ mmolL}^{-1}$  and channel ( $V_p$ )/cross flow ( $V_c$ ) ratio fixed at 0.5/0.8. Results are reported as the mean from 5 replicate analyses; the average standard deviation for the recovery and the retention ratio was 0.5 %

	Fixed molarity ratio CTAB : $\text{NH}_4\text{NO}_3$									
	5 % : 95 % (CL1)		30 % : 70 % (CL2)		50 % : 50 % (CL3)		70 % : 30 % (CL4)		100 % : 0 % (CL5)	
	R%	R	R%	R	R%	R	R%	R	R%	R
GNR1.4	81.5	0.052	101.5	0.056	72.37	0.069	57.4	0.076	38.8	0.084
GNR3.1	73.2	0.080	108.9	0.095	99.6	0.113	30.5	0.120	24.2	0.129
GNR3.8	7	0.086	87.7	0.112	79.3	0.130	37.3	0.133	22.5	0.139
GNR4.4	19.1	0.109	101.7	0.123	99.7	0.154	30.1	0.159	18.2	0.167

and 0.3 %, respectively. The values determined from the A4F traces represent the mean of 3 to 5 replicate injections, where the average coefficient of variation between replicate elutions (not shown) is less than 1 %



**Fig. 1** Typical DAD-based fractograms tuned at the appropriate TSPR wavelength position (550 nm, 710 nm, 780 nm and 850 nm) for the four different GNR samples (GNR1.4, GNR3.1; GNR3.8; and GNR4.4 respectively) realized with the same fractionation condition (10 kDa PES membrane, 350  $\mu\text{m}$  spacer thickness,  $V_p/V_c=0.5/0.8 \text{ mLmin}^{-1}$ ) as

a function of the  $\text{NH}_4\text{NO}_3/\text{CTAB}$  ratio (see Table 1) at a constant ionic strength of  $0.5 \text{ mmolL}^{-1}$  in the mobile phase: **a** CL1; **b** CL2; **c** CL3; **d** CL4. (\*): low signal amplified and normalized in order to compare with other fractograms. The red, black, blue and green lines correspond to GNR4.4, GNR3.8, GNR3.1 and GNR1.4, respectively

0.13. Additionally, the  $R$  values obtained with this mobile phase result in a Brownian (or normal) mode elution in A4F.

### Elution mechanism

Next, we evaluated the effect of the flow ratio on the retention behavior of GNR dispersions and their separation in the A4F channel. The influence of the applied  $V_c$  was investigated by examining the retention ratio, recovery, and the signal broadening characterized by peak width and height. As it was explained above (see Instrumentation and Methods),  $V_p$  was fixed at  $0.5 \text{ mLmin}^{-1}$  for the experiments and provided a good compromise between elution time and unacceptably high flow pressures, which indicates  $V_p$  is not the crucial parameter for fractionation in this case.

In this research,  $V_c$  was investigated over a range from (0.5 to  $3.0$ )  $\text{mLmin}^{-1}$ , but only a  $V_c$  range from (0.8 to  $2.3$ )  $\text{mLmin}^{-1}$  yielded an  $R$  value from 0.03 to 0.1, which is critical for normal mode elution. Notably, the recovery for all GNR samples obtained by this study of flow ratios revealed values equally high to those obtained with fixed  $V_c$  (i.e.,  $0.8 \text{ mLmin}^{-1}$ ) described above. This means that the optimized mobile phase system (CL2) is sufficiently robust for the characterization of GNRs regardless of the cross-flow rate chosen. In terms of peak broadening, Fig. 2 presents the variation of the DAD-based peak height at the corresponding TSPR position and width ( $\delta t_R$ ) for each tested GNR as a function of the applied  $V_c$ . Results show that even if no change in recovery is observed, a peak broadening effect appears above  $V_c \approx 1.8 \text{ mLmin}^{-1}$ . Above this value the peak width increases for all GNR samples, but particularly for GNR1.4. In other words, the peak broadening is inversely

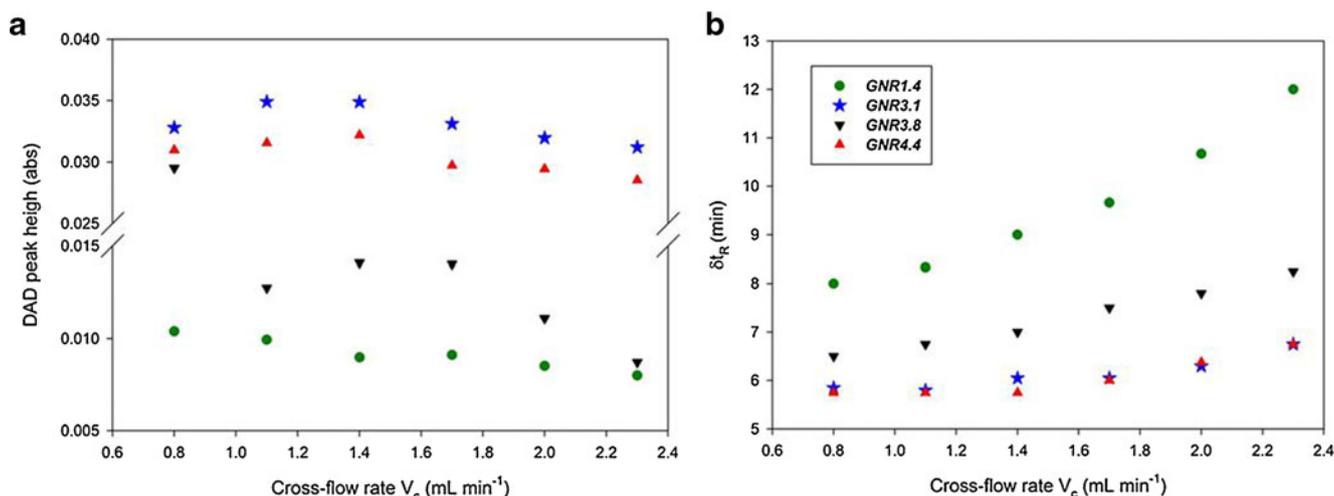
proportional to the aspect ratio, and this can be attributed to the lower retention ratio characteristic of the higher residence time in the channel yielding an excessive sample zone broadening.

With respect to the retention ratio obtained for different  $V_c$ , Fig. 3 presents the variation of  $R$  for the GNRs as a function of  $1/V_c$ ; a linear relationship between  $R$  and  $1/V_c$  is clearly apparent. According to Eq. (2), this linear relationship confirms the normal mode elution of GNRs, indicating the slope is directly proportional to the translational diffusion coefficient of the analytes under conditions where the spacer thickness is held constant and the void time is a determined quantity.

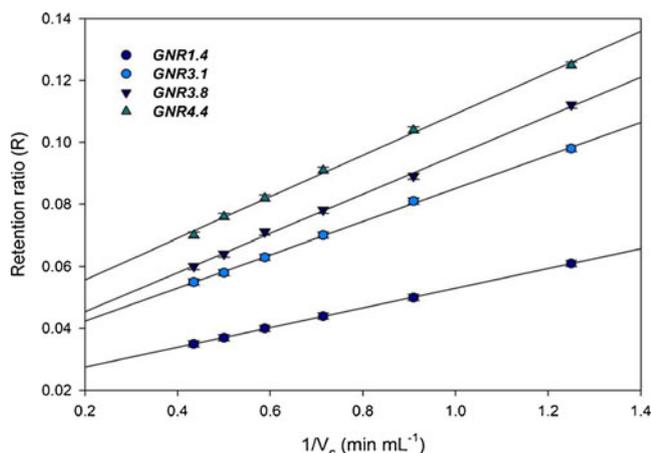
The diffusion coefficient for each GNR was determined by A4F measurement and the results are summarized in Table 3 (columns 1 and 2). The values obtained by a mathematical model are also described in Table 3 for comparison (columns 3 and 4). The mathematical model allows one to determine the diffusion coefficient for Brownian rods based on their size parameters (length  $L$ , diameter  $d$ , and aspect ratio  $L/d$ ), and is expressed in Eq. 4 [33, 34]:

$$D = \frac{kT}{3\pi\eta L} \left[ \ln\left(\frac{L}{d}\right) + 0.312 + 0.565\frac{d}{L} + 0.100\left(\frac{d}{L}\right)^2 \right] \quad (4)$$

Table 3 shows a general lack of consistency between the measured and calculated values when the FFF model for spherical particles is compared with the Brownian calculations; only in the case of GNR1.4, which is closest to spherical, do results agree statistically. In order to explain these differences, a theoretical study by Beckett and Giddings [1] can be used to rationalize the discrepancies. Indeed, these authors extended the general retention equation for FFF



**Fig. 2** Variation of the DAD peaks **a** height and **b** width for the GNR samples according to the cross-flow rate (the standard deviations for peak height and width are not shown, because they are smaller than the symbol size, i.e., of order 0.4 %)



**Fig. 3** Variation of the retention ratio for GNR samples as a function of the inverse cross-flow rate

normal mode elution to include a steric perturbation due to entropy associated with the orientation of non-spherical particles. In this typical mode of elution, perturbed by the steric-entropic contribution of the rod-like shape, Eq. (2) can be rewritten as [1]:

$$D = \frac{V_c \cdot \omega^2 \cdot R}{12 \cdot V_0} \tag{5}$$

In this case the “corrected” diffusion coefficient (labeled “non-spherical” in Table 3, column 2) is generally closer to those values obtained by the Brownian model. Nevertheless there remains a difference between corrected and calculated  $D$ , which may be explained by the low aspect ratio in the present study. In the literature [34], it has been shown by DLS characterization of GNRs that a significant deviation occurs between measured and calculated  $D$  for low aspect ratios ( $\leq 8$ ). These deviations could be attributed to the effect of the capping agent on the diffusion coefficient, because it contributes to the hydrodynamic radius. To test this, we applied the Brownian model using a reasonable approximation for the CTAB coating thickness ( $6.5 \pm 0.2$  nm). Results indicate that the difference between non-spherical FFF measurement results and the Brownian model decreases with the inclusion of the CTAB coating (the

exception being GNR3.1). This result suggests that the contribution of the CTAB coating is important, especially for low GNR aspect ratios. The residual deviation between  $D$  values (i.e., between the FFF results and the Brownian model), suggests that the separation is not only due to the diffusion coefficient, but that the aspect ratio, through its steric-entropic effect, also has an influence on the A4F separation process. Indeed,  $D$  determined by the Brownian model should depend on the length of the rod; however,  $D$  obtained by A4F measurements in this study are proportional to the GNR aspect ratio, and also  $R$  varies linearly with the corresponding aspect ratio (Fig. 4), without any clear relationship to rod length (Table 1).

Moreover, the separation process based on  $D$  and the aspect ratio in this investigation does not fully explain why longer GNRs with the same diameter (i.e.,  $GNR1.4$  and  $GNR3.1$  for diameter of 25 nm, and  $GNR3.8$  and  $GNR4.4$  for diameter of 10 nm) elute earlier than the shorter GNRs. These observations are inconsistent with previously reported results for flexible nanorods and nanotubes with high aspect ratio ( $\geq 100$ ), [18, 35, 36] where shorter lengths generally elute first.

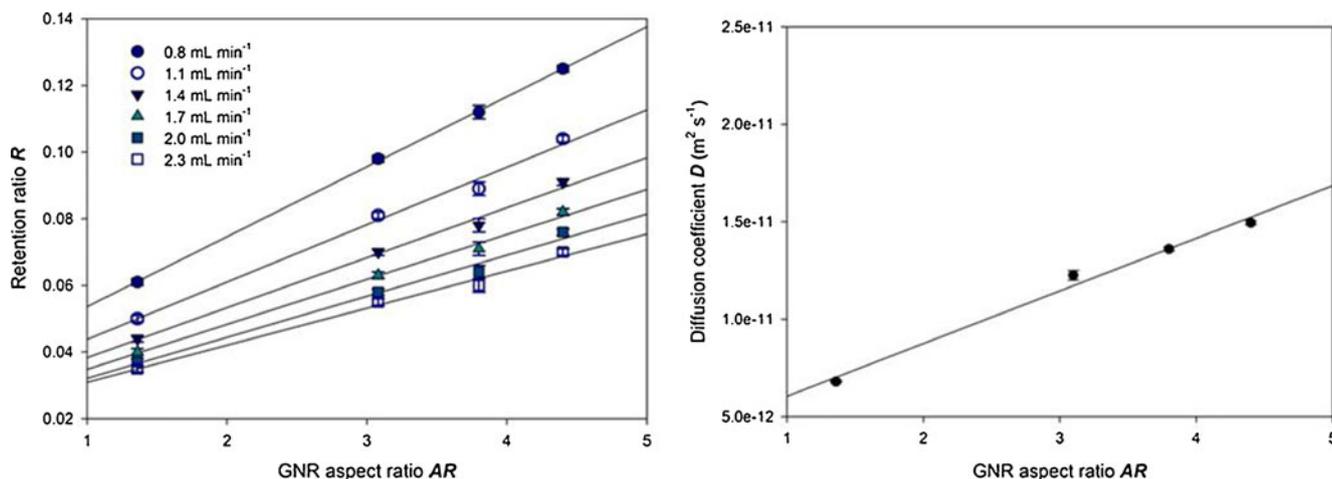
Adapted from the Beckett and Giddings theoretical framework for non-spherical particle elution, nanorods in the A4F channel, due to their steric-entropic contribution, can be assimilated to a unit sphere corresponding to the nanorod orientation vector (unit of length), which depends on the rod length and the distance from the accumulation wall. So, the concentration profile of the analyte in the sample for rod-like particles can be expressed as: [1]

$$c(x) = c_0 e^{-\frac{x}{l}} \left( 2 \frac{x}{L} \right) \tag{6}$$

The term,  $c(x)/c_0$  is the relative concentration of the analyte in the A4F channel,  $l$  is the mean layer thickness,  $x$  is the distance between the analyte and accumulation wall, and  $L$  is the rod length. Eq. (6) means that for rods with the same diameter, the longer rods have a concentration profile further removed from the accumulation wall compared to the shorter rods, and consequently elution is faster for longer rods independent of  $V_c$ . According to the parabolic velocity

**Table 3** GNR diffusion coefficients,  $D$  ( $\times 10^{-11} \text{ m}^2 \text{ s}^{-1}$ ), determined by A4F and calculated according to Eq. (4)

Sample	A4F measurement results FFF model		Calculated results Brownian model	
	Spherical [32]	Non-spherical [1]	Hard core size	With $6.5 \pm 0.2$ nm CTAB coating
<i>GNR1.4</i>	$1.36 \pm 0.01$	$0.68 \pm 0.01$	1.37	$0.58 \pm 0.10$
<i>GNR3.1</i>	$2.45 \pm 0.05$	$1.23 \pm 0.03$	0.91	$0.77 \pm 0.12$
<i>GNR3.8</i>	$2.72 \pm 0.02$	$1.36 \pm 0.01$	1.98	$1.41 \pm 0.15$
<i>GNR4.4</i>	$2.99 \pm 0.02$	$1.50 \pm 0.01$	1.88	$1.34 \pm 0.17$



**Fig. 4** Representation of **a** variation of GNR retention ratio as a function of the aspect ratio, and the **b** variation of GNR diffusion coefficient determined by A4F also as a function of aspect ratio

profile of the channel flow, particles located higher in the channel elute faster than those closer to the membrane surface. This explains why, in the case of GNRs with the same diameter but different lengths, the longer GNRs elute first.

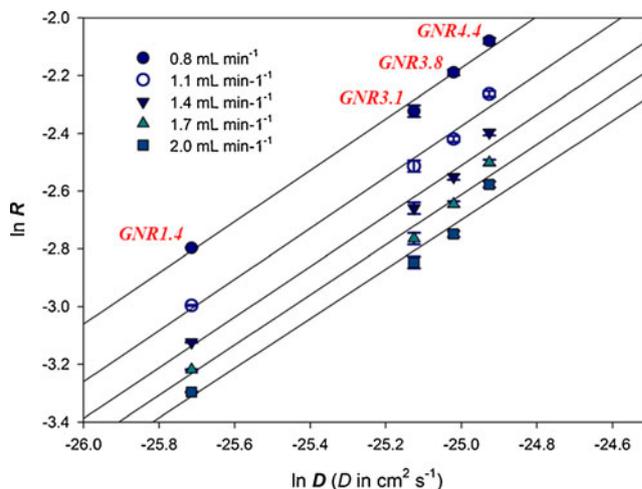
Nevertheless this theory does not explain why, in the case of GNR3.1 and GNR3.8, with different diameters, the shorter length rods (GNR3.8, length of 38 nm) elute earlier than the longer rods (GNR3.1, length of 77 nm). In this particular case the theory from Beckett and Giddings is not consistent with the results; however, it is possible to explain this phenomenon based on the GNR aspect ratio without needing to consider separately the diameter and/or the length. As the elution occurs in normal mode (i.e., a linear relationship exists between  $R$  and  $D$ ), in the small aspect ratio and nanoscale size range, the aspect ratio is the dominant parameter that controls elution of GNRs without needing to consider separately the diameter and/or the length. The theory for the elution of non-spherical particles works best for particles with the same diameter and the same distance from the accumulation wall [1]. The A4F results reported here suggest that the elution of GNRs depend on:

- 1) GNR aspect ratio, with a linear relationship that is insensitive to the cross-flow,
- 2) GNR steric-entropy contribution associated with their orientation (for the same diameter but different length).

As mentioned above, the experimental results in this study reveal different but interesting phenomena beyond the classical hard-sphere theory. More specifically, that the retention of asymmetric, but low aspect ratio, nanoparticles (in this case GNRs), under a particular experimental condition, depend directly on the diffusion coefficient and correlated particle shape (aspect ratio), rather than on the rod length alone. Based on the novel concept of separation by

shape instead of size, the capability of A4F was tested not only for characterization of GNRs, but also for separation of individual GNRs from a mixture. Furthermore, the high sensitivity of retention to the relatively small aspect ratio of GNRs (less than 5) used in this study suggests the potential for exploitation of subtle shape-dependent fractionation of nanoparticles, an effect we are exploring for a future publications.

In order to conduct shape-based separation by A4F, the quality of fractionation should be evaluated. Hence, we preliminarily propose to adopt a definition of “selectivity” for shape fractionation derived from classical FFF theory, in which selectivity is defined as “a measure of the inherent ability of a technique to separate two components” [32]. In a manner consistent with the basis for classical selectivity determination in A4F (i.e.,  $t_R$  and hydrodynamic diameter), we propose to define shape characterization selectivity ( $S_D$ )



**Fig. 5** Representation of  $\ln R$  versus  $\ln D$  for GNRs over the range of  $V_c$  tested in this study

as a function of  $D$  (as it has been demonstrated that GNR diffusivity is linearly proportional to the aspect ratio) and  $R$ , such that: [32]

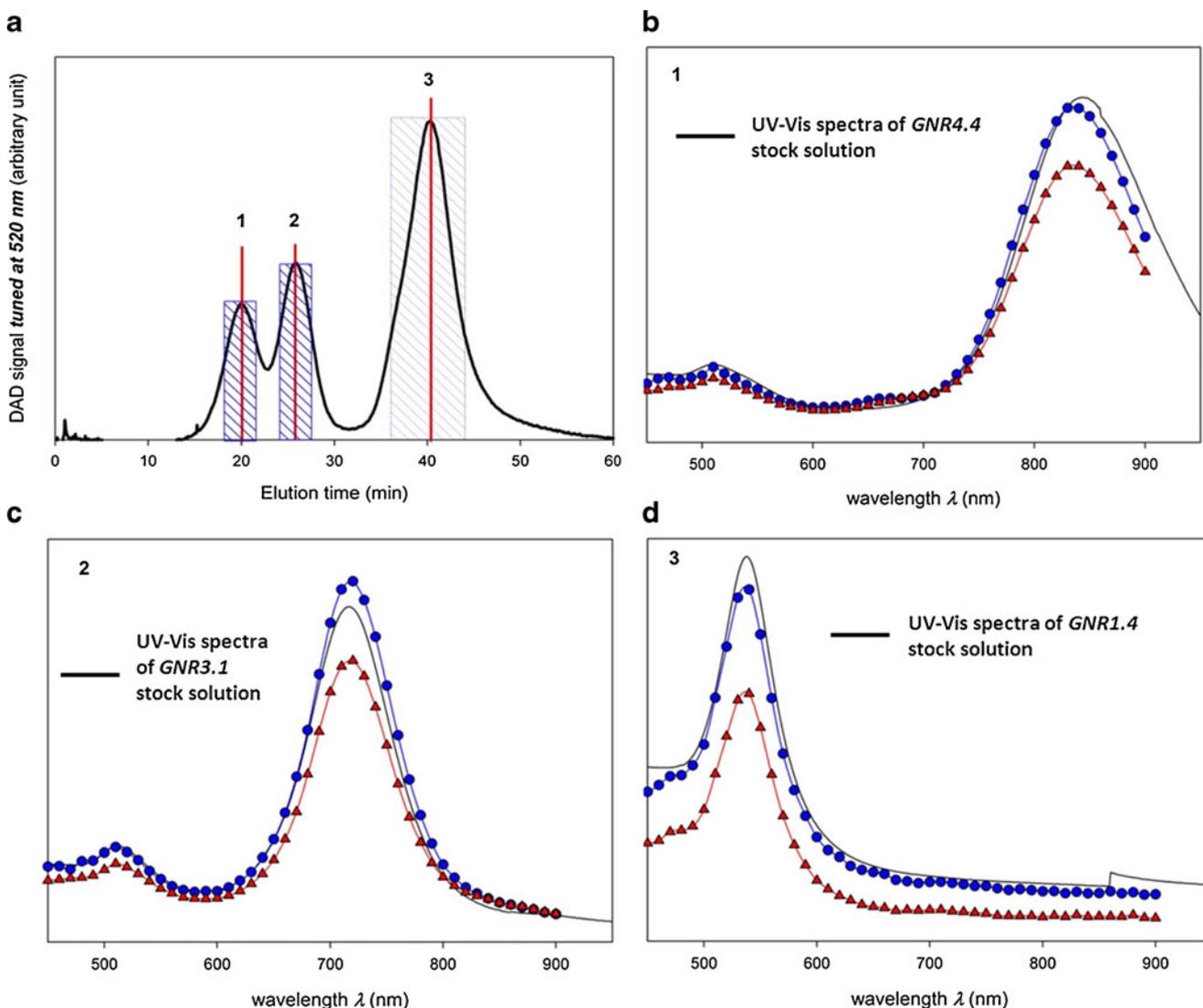
$$S_D = \left| \frac{d \ln R}{d \ln D} \right| \quad (7)$$

In A4F, separation depends on the diffusion coefficient of the analytes, so that the highest  $S_D$  that can be obtained is close to unity [32]. As illustrated in Fig. 5, by plotting  $\ln R$  versus  $\ln D$  at various cross-flow rates, the relationship is linear, and, according to Eq. (7), the slope of this relationship is equal to  $S_D$ . For  $V_c$  ranging from (0.8 to 2.0) mL  $\text{min}^{-1}$ ,  $S_D$  ranges from 0.857 to 0.888, respectively. These  $S_D$  values are close to unity and confirm the efficiency of the

method for separating GNRs according to their shape. Indeed, as it was explained previously, the selectivity describes the ability of the technique to fractionate one sample without consideration of its polydispersity and complexity. So a convenient  $V_c$  range should be chosen that enables an acceptable selectivity, then an appropriate  $V_c$  must be selected for the particular mixture to be investigated, such that the highest possible resolution and recovery are attained.

#### Validation and applicability

We evaluated the efficiency of the method developed in this investigation for separation and characterization of GNR



**Fig. 6** **a** Typical fractograms obtained at the optimal fractionation condition (10 kDa PES membrane, 350  $\mu\text{m}$  spacer thickness,  $V_c=2.0$  mL  $\text{min}^{-1}$ ,  $V_p=0.5$  mL  $\text{min}^{-1}$  and CL2 mobile phase) for the 3-component GNR mixture (black line) with DAD tuned to 520 nm; **b** to **d** the UV-vis spectra measured on-line for GNRs corresponding to the

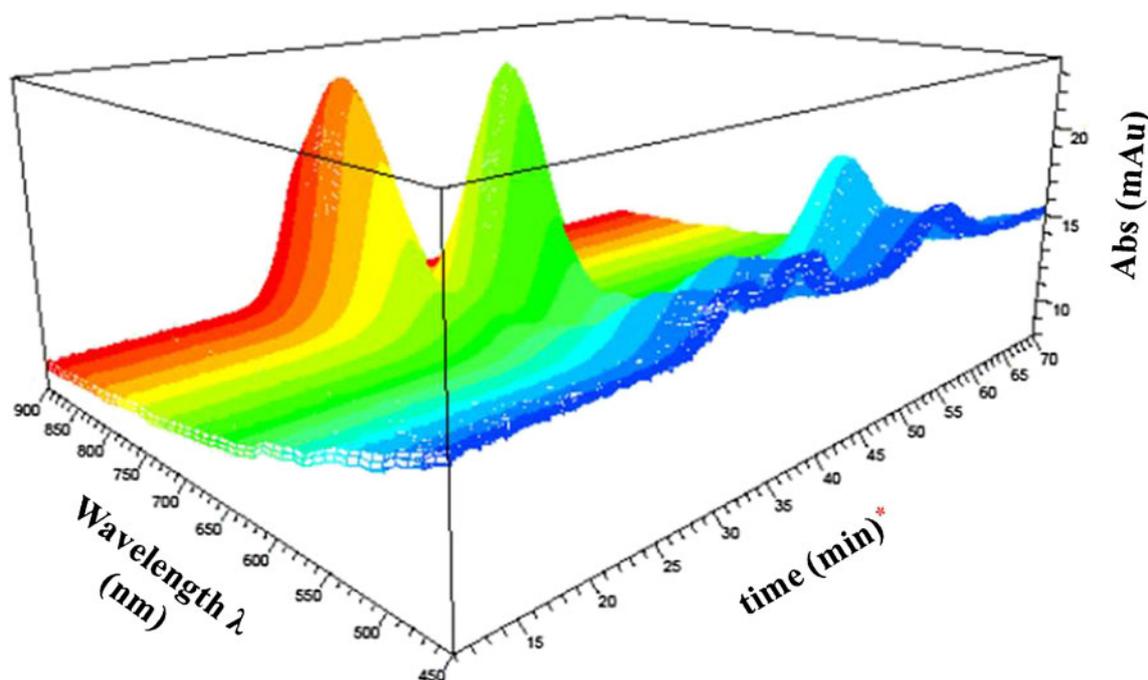
3 peaks (marked 1,2 and 3 in a) at the top of the signals (blue line, circles) and the peak-averaged spectrum (red line, triangles), and the UV-vis spectra of the different GNR native suspensions (black line, no symbols)

mixtures. A mixture of three GNRs (*GNR1.4*, *GNR3.1* and *GNR4.4*) was prepared by maintaining the same dilution factor. In order to obtain three distinct signals, several elution conditions were tested, and the highest resolution with minimal loss of material to the membrane surface was achieved, with  $V_c=2.0 \text{ mL min}^{-1}$ . The observed fractogram for the mixture, traced using an absorption wavelength of 520 nm, is illustrated in Fig. 6. Additionally, the UV–vis spectrum for each individual peak was measured on-line at two retention times: one spectrum at  $t_R$  corresponding at the maximum of the peak and a second spectrum averaged over the whole peak area (average spectrum calculated by the software). These spectra are then compared to the UV–vis spectra obtained for the corresponding individual GNR stock solutions (i.e., unmixed). It appears that all UV–vis spectra correspond correctly and that co-elution of GNRs is not occurring in the mixed system. Furthermore, no difference is observed between the peak-averaged spectrum and the spectrum taken at the top of the peak. Combined, these results confirm that the A4F method can separate individual monodisperse GNRs within a mixture, even where the differences in aspect ratio are relatively small. The UV–vis spectra obtained on-line for the different trace peaks, and compared to the spectra for GNR stock solutions, allow us to identify the different populations beyond any reasonable doubt. Moreover the individual GNR components exhibit the same absorbance spectral characteristics and corresponding retention times as the native GNR suspensions (Fig. 6). Thus,

single wavelength DAD detection at 520 nm, for this mixture, is sufficient to confirm the successful separation of the component GNRs. Our results also indicate there is no significant interparticle interaction between GNRs (which would result from chemical and/or physical interactions) in the mixed state or during the A4F measurements, respectively; such interactions would likely manifest themselves by the appearance of agglomerates.

Also, as all absorbance signals are identified for the different GNRs, it is possible to determine the selectivity; a very reasonable selectivity of 0.87 was obtained for this mixture. This indicates that the methodology developed in the present study has similar separation efficiencies for GNRs either as individual components or in complex mixtures.

It is well documented that for GNRs and gold nanoparticles alike, changes in the SPR bands can be observed upon changes in the aggregation state, and it was therefore necessary to check that no interaction occurred during the elution process that would alter the effective aspect ratio and size of the GNRs. Additionally, to support further confirmation of the identities of observed signals for the GNR mixture (see above), A4F measurements were conducted using a range of absorbance wavelengths. The resulting fractograms are represented in 3-dimensional (3D) format in Fig. 7. The fractograms collectively exhibit three peaks corresponding to the three GNR components. It appears that each peak position (along the retention time



**Fig. 7** 3D representations of typical A4F fractogram (two different orientations) obtained for the GNR mixture using different optical absorbance wavelengths. Time represented here includes a focus and

injection step of 11 min; therefore, to compare with previous reported elution times it is necessary to first subtract 11 min

axis) is constant, but the peak intensity changes depending on the wavelength observed. The peak located at lower retention time ( $t_R=19.8$  min) has a higher intensity at 844 nm, which corresponds to the GNR4.4 longitudinal SPR band ( $\lambda_{\max}=844$  nm). A similar observation can be made for the second peak at a wavelength of 712 nm, which corresponds to GNR3.1 ( $\lambda_{\max}=712$  nm). Finally, for GNR1.4, with a longitudinal SPR band ( $\lambda_{\max}=550$  nm), the overlapping longitudinal (550 nm) and transverse (520 nm) bands correspond to the peak with the highest retention time. This result again demonstrates that the method allows separation of GNRs according to their aspect ratio. Additionally, in the 3D fractogram example (Fig. 7), no peaks were observed at wavelength positions that might indicate the presence of other morphologies resulting from the interaction of GNRs during focusing and elution.

It is worthwhile comparing characterization of the GNR mixture by A4F-DAD with that obtained in batch mode (i.e., “one pot analysis”) using an off-line UV–vis spectrometer; even if the batch mode spectrum yields evidence of multiple GNR components present in the sample, it does not permit discrimination between different populations (especially for GNRs with a small aspect ratio). The lowest GNR aspect ratio (slightly above unity) has a longitudinal SPR band around 550 nm, close to and overlapping with the transverse mode at 520 nm common to all GNRs. So, here it is possible using the A4F-DAD method to separate and characterize GNRs with aspect ratios ranging from very small (close to spherical) to much higher values (more rod-like).

## Conclusions

In this work, a novel application of A4F was demonstrated for the characterization of CTAB-stabilized GNRs based on their aspect ratio. We showed the capacity for A4F to fractionate positively charged nanoparticles (with pH in the range 3 to 4). The problem of irreversible adsorption of positively charged nanoparticles onto the A4F accumulation wall (negatively charged membrane) can be eliminated by controlling the mobile phase composition (e.g., the ratio between ammonium nitrate and CTAB, and ionic strength). The optimized condition affords a convenient retention time associated with the highest possible recovery. We then described and validated an A4F methodology that permits eluting GNRs according to their shape (i.e., aspect ratio). We believe this to be the first reported experimental study to clearly show the steric-entropic contribution of nanoparticle shape to the elution process by FFF, where the GNR diffusion coefficient, aspect ratio and orientation vector controls elution in normal mode A4F. This result, in accordance with FFF theory, is different from those obtained

in previous studies of nanowires and carbon nanotubes reported in the literature, where particles with the lowest aspect ratio eluted before the higher aspect ratio particles [18, 37]. Finally, we applied the developed methodology to fractionate GNR components within a complex mixture containing different aspect ratios. The results show that multi-wavelength optical absorbance detection can be relevant to interpret the shape of GNRs according to their retention time in A4F. The combination of absorbance detection with A4F has the advantage of in situ analysis (compared to, e.g., electron microscopy) to investigate GNR shape (aspect ratio) and to separate individual populations.

Further studies are required to evaluate the application of this method to characterize more complex mixtures of GNRs and other asymmetric nanoscale objects, and under a wider range of dispersion conditions. Additionally, we will expand this work to investigate tubular geometries with aspect ratios similar to the rod-like geometry studied here, and to demonstrate the broader applicability of the aspect ratio dependent elution behavior described in this work.

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